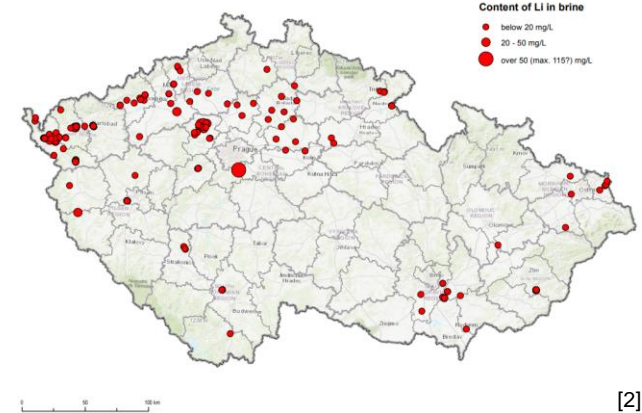
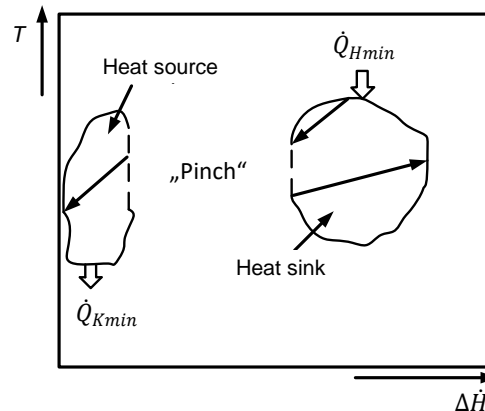


# Utilisation of energy from highly mineralised deep geothermal brines as part of material co-production of minerals



Wroclaw, 04.12.2024

# Geothermal potential from heat source to sink

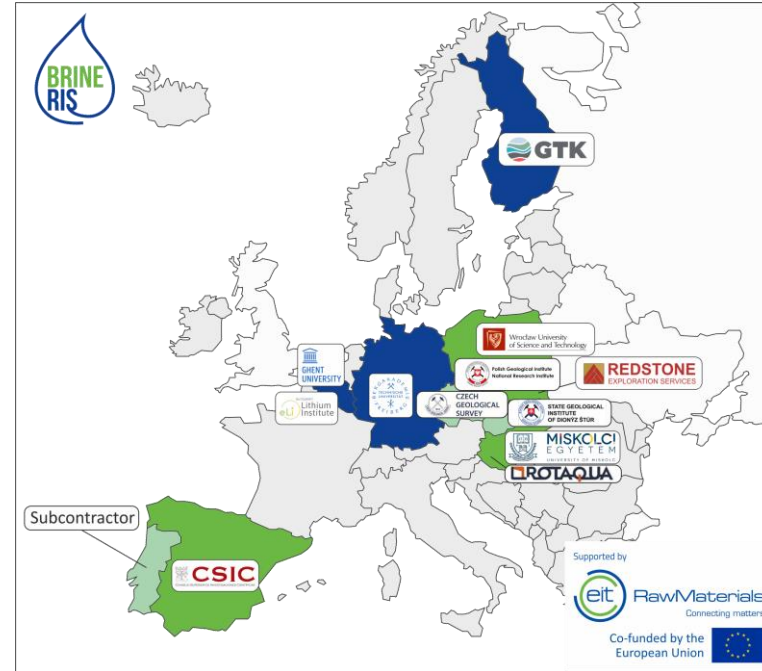
- Collection of a brine database



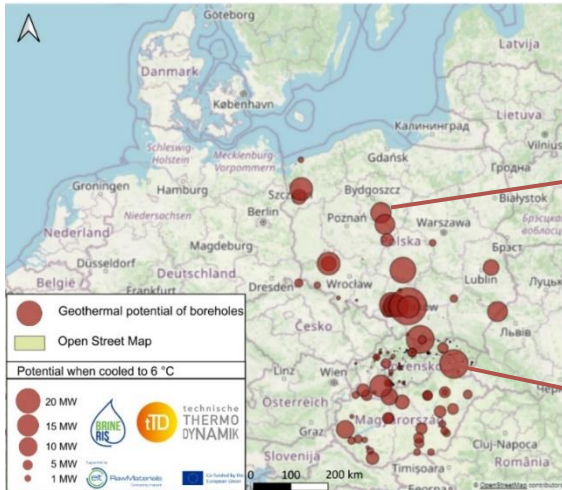
- Combination of brine recovery processes and utilisation of heating and cooling potentials



- Forcing ahead with European lithium production



# Geothermal potentials



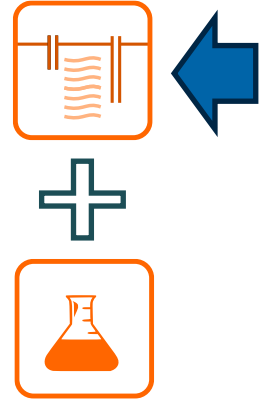
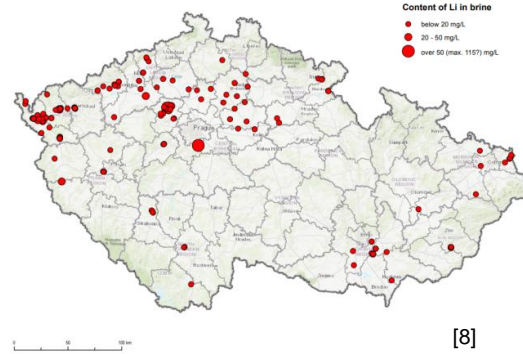
Name: PO-S6  
 Country: PO  
 Longitude: 2.044e+6  
 Latitude: 6.937e+6  
 Li: 0.24 mg/l  
 Mn: 0.17 mg/l  
 Temperature: 29.90 °C  
 Flow: 141.24 kg/s

Name: SK-S302  
 Country: SK  
 Longitude: 2.386e+6  
 Latitude: 6.228e+6  
 Li: 36.80 mg/l  
 Mn: 0.05 mg/l  
 Temperature: 125.00 °C  
 Flow: 55.83 kg/s  
 Geoth. Pot. (->6°C): 27838.39 kW



# Example location in the Czech Republic (HP-13)

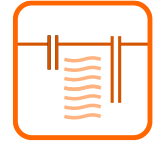
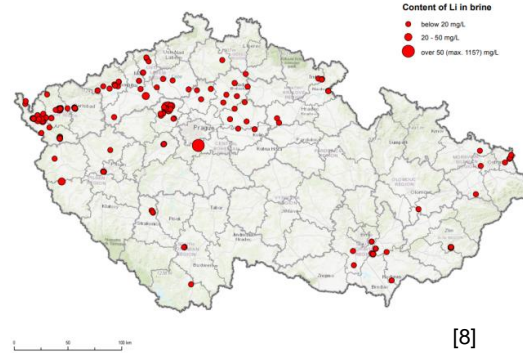
	value
Lithium content [mg/l]	47,00
Temperature [°C]	10,50
Volume flow [m <sup>3</sup> /h]	11,09



Mass flow (kg/s)	Heating potential (kW) cool down 5 K	Heating potential (kW) cool down 15 K	Maximum Amount of Heating Energy (MWh/a 5 K)	Maximum Amount of Heating Energy (MWh/a 15 K)
3,67	76,8	0	672,6	0

# Example location in the Czech Republic (HP-13)

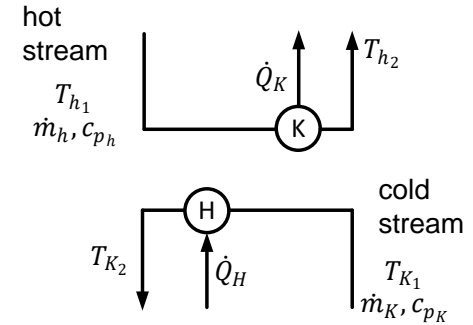
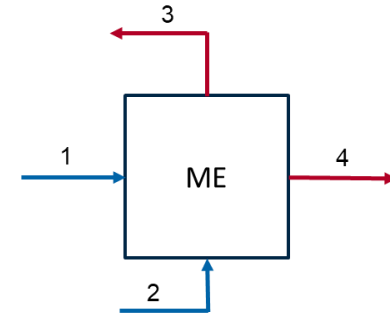
	value
Lithium content [mg/l]	47,00
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Mass flow (kg/s)	Heating potential (kW) cool down 5 K	Heating potential (kW) cool down 15 K	Maximum Amount of Heating Energy (MWh/a 5 K)	Maximum Amount of Heating Energy (MWh/a 15 K)
3,67	76,8	0	672,6	0

# Wärmeintegration

- Analysis of systems with flows that can heat up or cool down differently
  - The analysis using heat integration should provide the following information:
    - Recognise the minimum required useful energy demand
    - Heat integration potential
    - Determination of the minimum heating and cooling requirements
    - Minimum exergy loss
- ➔ Method: Pinch analysis!

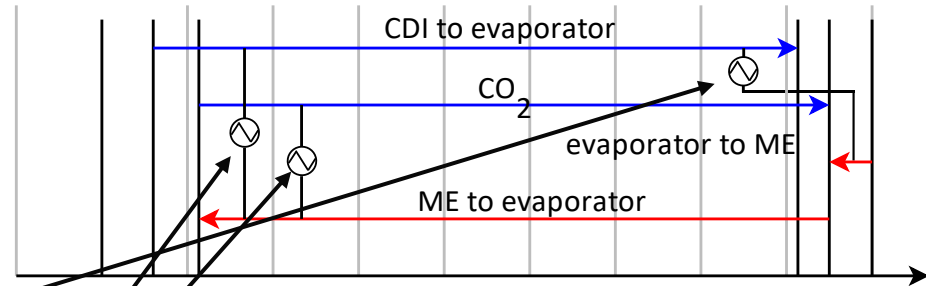


# Wärmeintegration

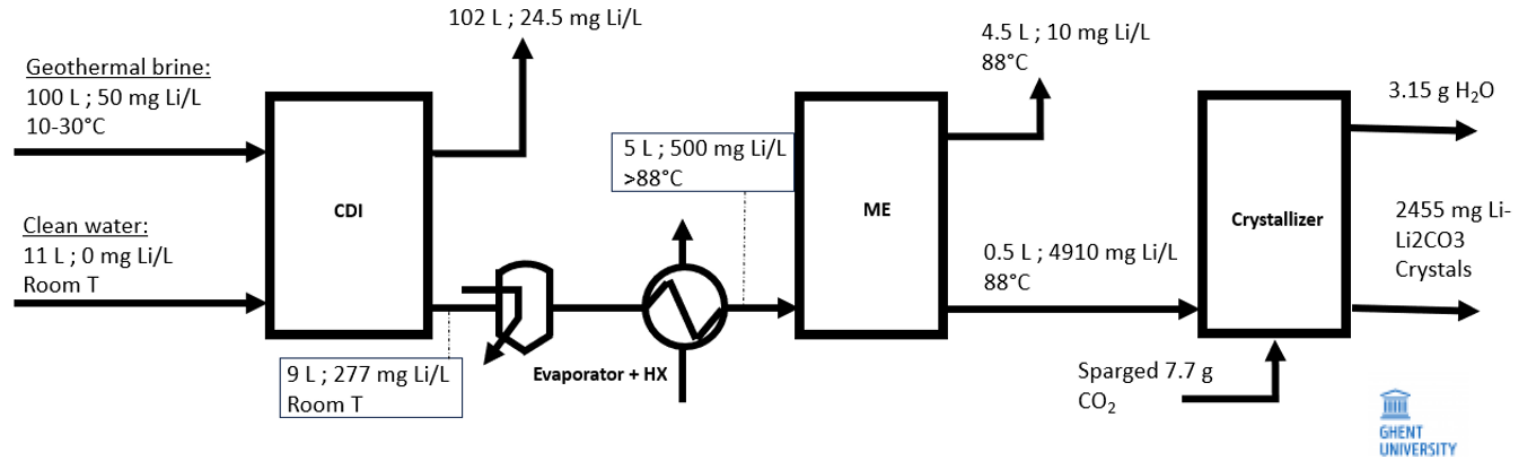
- Interconnection of hot and cold flows
- Aim: efficient utilization

## Interconnection flows

- Cool down with 100 °C to 95 °C
- Preheat with 100 °C to 93 °C
- Cool down from 95 °C to minimum
- Preheat with 95 °C to 88 °C
- Preheat with 47 °C to 30 °C



# Example process of the University of Ghent



Black box model for lithium extraction, incomplete material flows (2024)



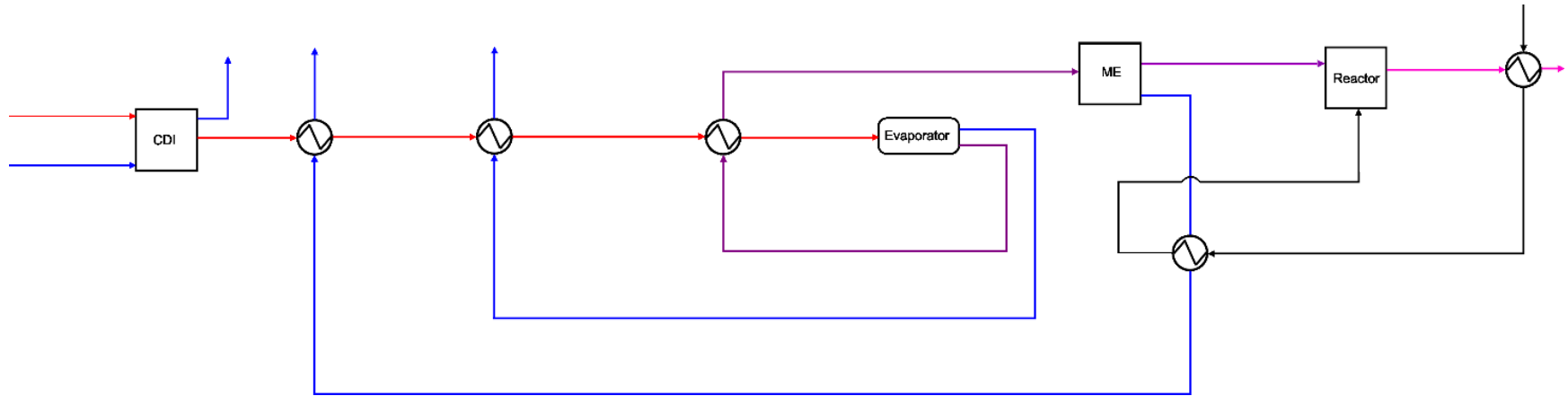
# Starting Situation

- Integrating the streams
- options after/before each process



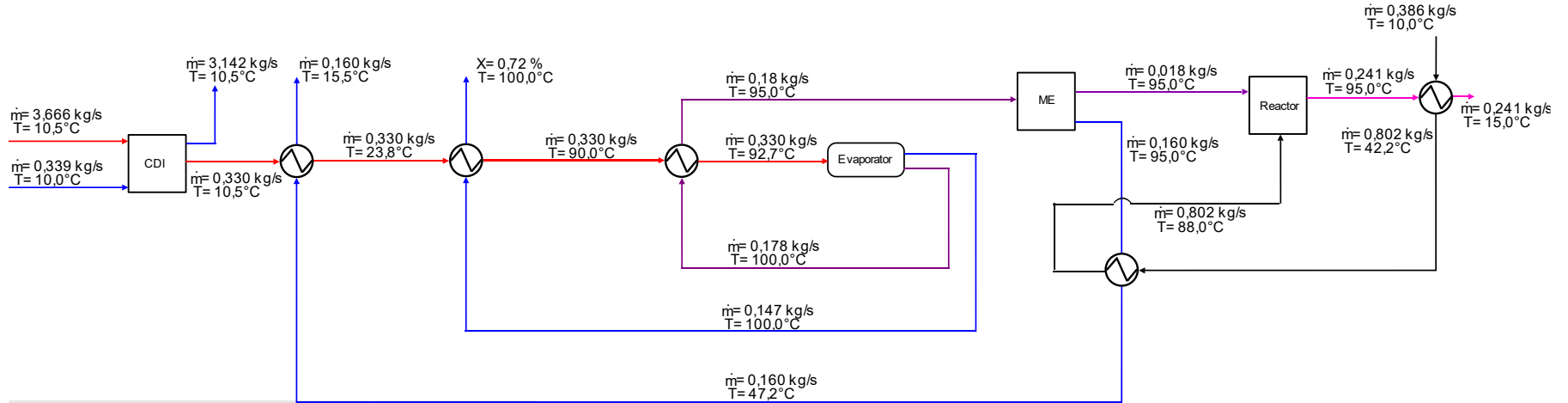
→ Brine solution → water → concentrated brine → CO<sub>2</sub>

# Interconnected Process



→ Brine solution → water → concentrated brine → CO<sub>2</sub>

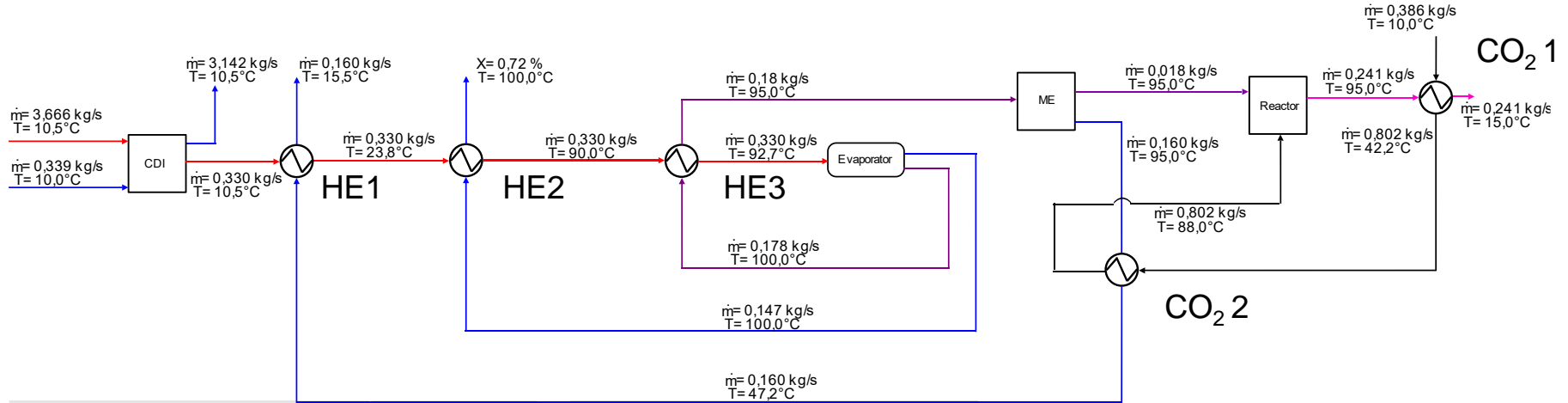
# Process for the location in the Czech Republic



	value
Lithium content [mg/l]	47,00
Temperature [°C]	10,50
Volume flow [m³/h]	11,09

→ Brine solution → water → concentrated brine → CO<sub>2</sub>

# Process for the location in the Czech Republic

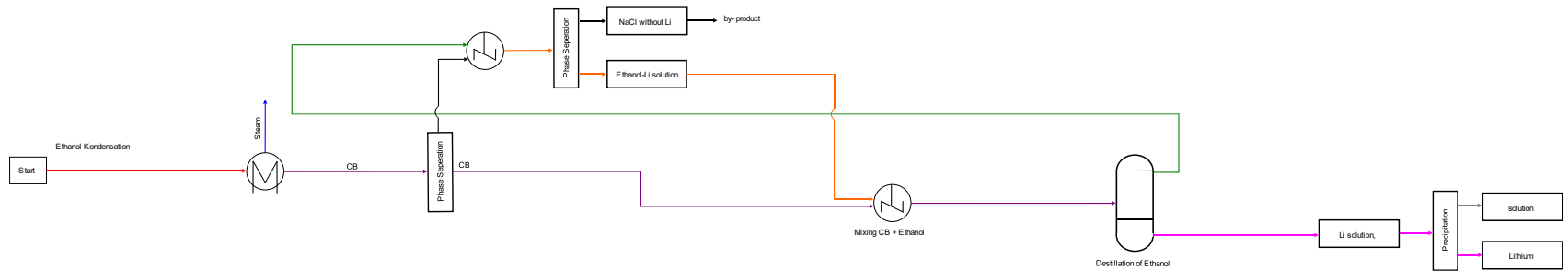


	value
Lithium content [mg/l]	47,00
Temperature [°C]	10,50
Volume flow [m³/h]	11,09

Heat exchangers		
HE brine 1	18,42	kW
HE brine 2	91,54	kW
HE brine 3	3,73	kW

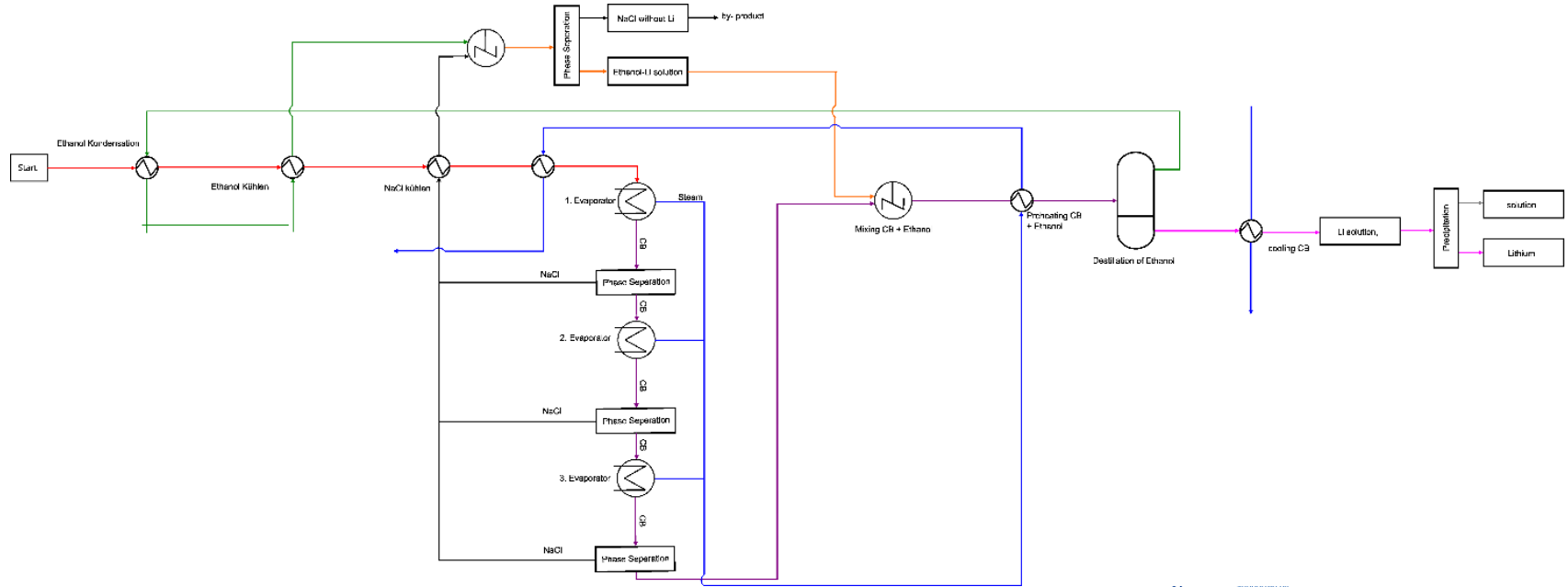
Heat exchanger		
HE CO <sub>2</sub> 1	21,77	kW
HE CO <sub>2</sub> 2	32,12	kW

# Solvent Extraction (SX)



- Evaporation of the brine
- Solid is mixed with fluid
- Mixture of concentrated brine and fluid solution
- Distillation
- Final product

# Solvent Extraction (SX)

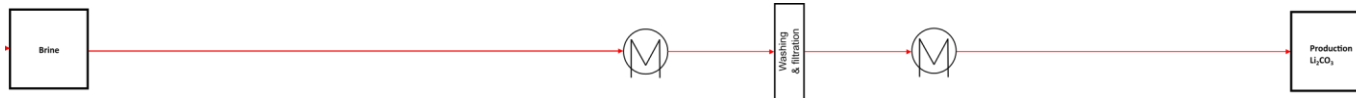


# Synthetic adsorption

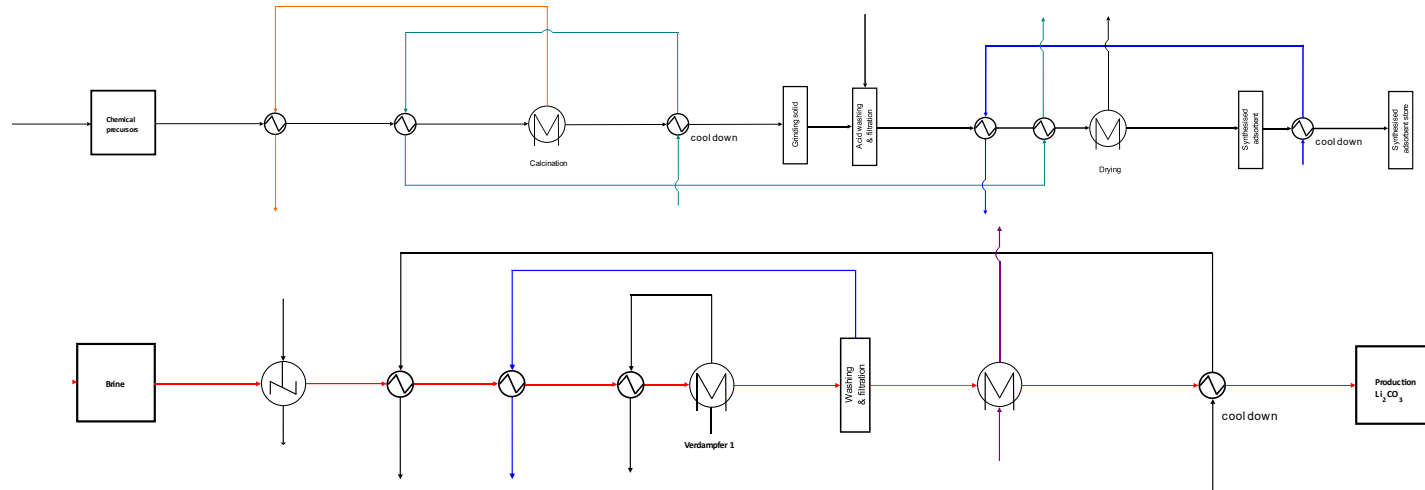
- Production of an adsorbent



- Reaction of adsorbent and brine
- Vaporisation of the liquid



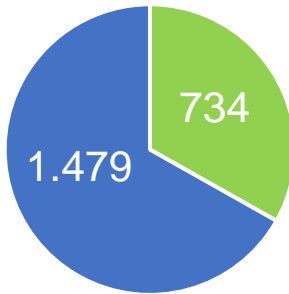
# Synthetic adsorption





# Energy demand

## Membrane electrolysis

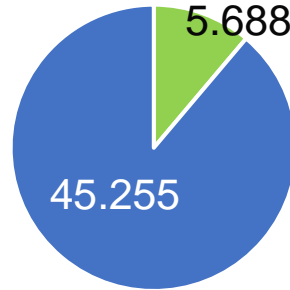


- Energy-saving MWh/a
- Energy Demand MWh/a

Total 2.212 MWh/a

Savings 33,2 %

## Solvent Extraction

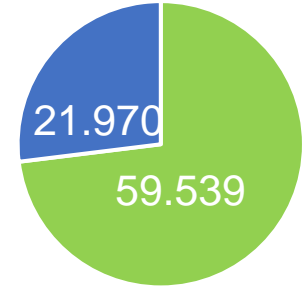


- Energy-saving MWh/a
- Energy Demand MWh/a

Total 50.943 MWh/a

Savings 11,2%

## Synthetic adsorption

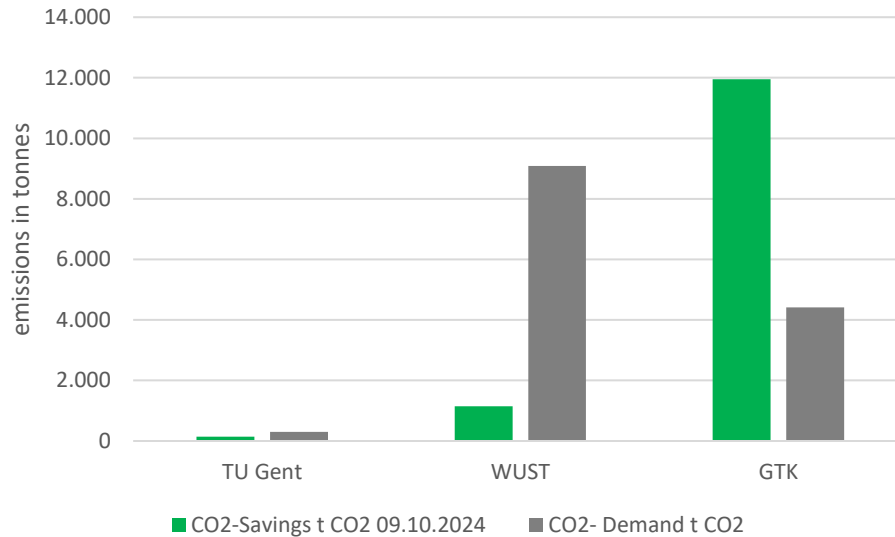


- Energy-saving MWh/a
- Energy Demand MWh/a

Total 81.509 MWh/a

Savings 73,0%

# CO<sub>2</sub>- Emissions






- According to energy consumption, there are clear differences
- The calculation is based on a factor of 200.8 g CO<sub>2</sub>/kWh natural gas equivalent

# Location in the Czech Republic (HP-13)

Figure		Membrane electrolysis	Solvent Extraction	Synthetic adsorption
Energy Demand	MWh/a	734	5.688	59.539
Energy-saving	MWh/a	1.479	45.255	21.970
Energy-saving	%	33,2	11,2	73,0
CO <sub>2</sub> - Demand	t CO <sub>2</sub>	147	1.142	11.956
CO <sub>2</sub> -Savings	t CO <sub>2</sub>	297	9.087	4.412
Cooling Potential	MWh/a	270	0,00	0,00
Heating Potential	MWh/a	1.423	30.556	0,00
Lithiumcarbonat	kg/a	≈1.800 (±20%)	≈1.730 (η= 76%) [12]	missing data from the lab

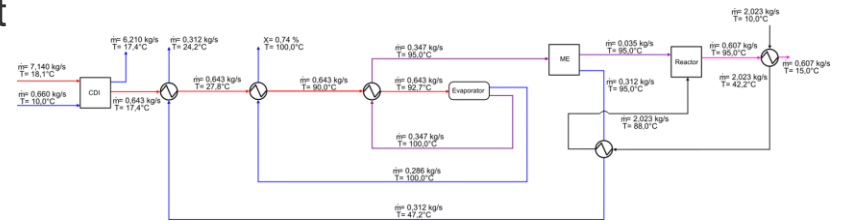
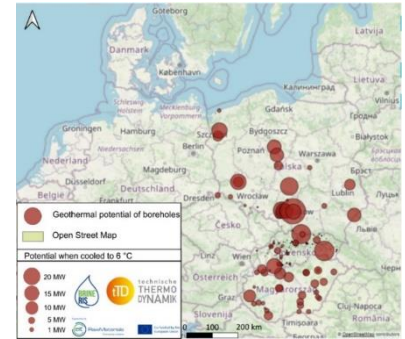
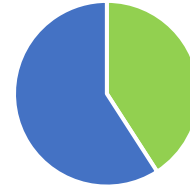
# Comparison to 1 kg end product

	Membrane electrolysis	Solvent Extraction	Synthetic adsorption
	energy/ 1 kg kWh		
	Cost <sub>fossil</sub> / 1 kg €		
	Cost <sub>renew</sub> / 1 kg €		No data available from the lab
	CO <sub>2-fossil</sub> / 1 kg kg		
	CO <sub>2-renew</sub> / 1 kg kg		

Assumptions Czech Republic :  
 Gas costs: 0.11 €/kWh  
 Electricity (not private): 0.21 €/kWh  
 Electricity (CO2 factor): 107g CO<sub>2</sub>/kWh  
 COP heat pump: 4

# Conclusion

- Calculated values:
  - Geothermal potential determined
  - Energy savings
  - CO2 cost
  - Lithium available
- Process analysed (processes currently at laboratory scale)
- Lithium production in Europe possible





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