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Critical review of polymer membranes with crown ethers for lithium extraction

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The CompLithium project - Complex technology for lithium and potable water recovery from produced waters



The aim of the project is to develop a technology for the recovery of lithium and potable water from waste reservoir brines based on combined sorption-membrane techniques. The proposed solution is a process innovation on a national and global scale. The elements of the novelty are:

- high-porosity sorbents made with the 3D printing technique for lithium recovery with improved selectivity and sorption capacity;
- nanofiltration membranes modified with crown ethers for the simultaneous production of desalinated water and sorption of residual lithium from brines.



Lithium concentration in produced waters as a function of total dissolved solids, potassium concentration, magnesium concentration and reservoir pressure



	К	Na	Mg	Ca	Li	рН	TSS	TDS	OC	WP	RP	GP	WPW
К	1.00												
Na	0.20	1.00											
Mg	0.74	-0.01	1.00										
Ca	0.39	0.46	0.15	1.00									
Li	0.87	0.21	0.41	0.37	1.00								
рН	-0.07	-0.32	-0.13	-0.35	0.10	1.00							
TSS	0.39	0.15	0.01	0.33	0.43	-0.07	1.00						
TDS	0.62	0.79	0.44	0.79	0.51	-0.40	0.30	1.00					
OC	0.32	-0.20	0.28	0.19	0.22	-0.18	0.29	0.09	1.00				
WP	-0.05	-0.26	-0.08	-0.28	0.00	0.42	0.01	-0.28	-0.19	1.00			
RP	0.29	0.00	-0.05	0.16	0.54	0.02	0.21	0.07	0.04	-0.11	1.00		
GP	-0.39	-0.50	-0.28	-0.46	-0.31	0.34	-0.12	-0.60	-0.02	0.44	-0.12	1.00	
WPW	0.12	-0.03	-0.08	-0.12	0.22	0.35	0.05	-0.10	-0.18	0.22	0.42	0.29	1.00

Correlation matrix between selected parameters

OC – oilfield chemistry, WP – water production, RP – reservoir pressure,

GP – gas production, WPW – number of wells producing water



Crown ether is a sort of macrocyclic ligand possessing excellent complexing affinity to metal ions, which is able to form complexes through ion-dipole interaction of the negatively charged oxygen atoms with metal ions (in particular alkali metal and alkali earth metal ions) positioned in the center of the crown ether ring. Li⁺ has an ionic diameter of 1.36 Å, which matches best the cavity size of 14-crown-4.



The interactions between dibenzo-14-crown-4 ether functionalized with an alkyl C16 chain and Li⁺

> Strong electrostatic interaction

van der Waals interaction Strong repulsion (Steric effect) Table 1. Calculated geometric parameters of the complexes formed between DB14C4-C16 and Li⁺, Na⁺, K⁺, Ca²⁺, and Mg²⁺.

Bond (M-O)	Li+-O	Mg ²⁺ -O	Na ⁺ -O	Ca ²⁺ -O	K+-O
Length (Å)	1.94-1.95	2.02-2.04	2.25-2.26	2.49-2.54	2.64-2.67

Table 2. Thermodynamic analysis results of the complexes formed by Li⁺, Na⁺, and Mg²⁺ with DB14C4-C16 and H₂O.

Complex	ΔH (kJ/mol)	ΔG (kJ/mol)	ΔE (kJ/mol)	ΔS (kJ/mol/K)
DB14C4-C16-Li ⁺	-162.548	-125.813	-160.08	-0.12301
DB14C4-C16-Na ⁺	-90.2907	-55.7309	-87.8222	-0.1159
DB14C4-C16-Mg ²⁺	-241.04	-196.02	-238.572	-0.15104
H ₂ O-Li ⁺	-65.6051	-40.6078	-63.1294	-0.08368
H₂O-Na⁺	-49.4214	-25.3559	-46.9428	-0.08075
H ₂ O-Mg ²⁺	-98.557	-71.4908	-96.0789	-0.09079





2-Hydroxymethyl-12-crown-4

Synonym(s): (12-Crown-4)-2-methanol, 1,4,7,10-Tetraoxacyclododecan-2-methanol

Empirical Formula (Hill Notation): C₉H₁₈O₅

CAS No.:	75507-26-5	Molecular Weight:	206.24
EC No.:	278-224-5	Beilstein No.:	<mark>4661968</mark>

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Reaction scheme for graphene oxide synthesis





Stage 2



Scheme of graphene oxide modification with epichlorohydrin

2-Hydroxymethyl-12-crown-4, which is commercially available, was used as a reference crown ether in the modification of graphene oxide. However, from the study on lithium capture selectivity of various crown ethers, it is known that the 12-crown-4 ring is less selective in comparison to the 14-crown-4 ethers. The selectivity coefficient of Li⁺/Na⁺ separation in model system is equal to 1.7 for the 12-crown-4 and 20 for the 14-crown-4.



Reaction scheme for hydroxy-DB14C4 synthesis





Reaction scheme for introduction of dibenzo-14-crown-4 onto the modified GO







XRD patterns of raw graphite, graphene oxide and GO after epichlorohydrin and crown ethers immobilization.

SEM images of (a) raw graphite, (b) graphene oxide, (c) GO modified with epichlorohydrin, (d) GO modified with epichlorohydrin and 2-hydroxymethyl-12-crown-4.



Two series of experiments were performed, the first using pure lithium chloride solution with a lithium concentration of 200 mg/L and the second with real brine containing approx. 200 mg/L of lithium ions. The results presented in Table below include the recovery and operating capacity measured at pH 5 and pH 8 for various materials contacted with the brines at a solution to material mass ratio equal to 10/1.

Sampla nama	R Li*	R Brine**	q Li*	q Brine**
Sample name	(R Li pH 8)	(R Brine pH 8)	(q Li pH 8)	(q Brine pH 8)
GO	28% (45%)	2% (4%)	0.89 (1.47)	0.05 (0.08)
GO-Epi2	75% (62%)	6% (2%)	1.96 (1.67)	0.17 (0.05)
E1 (2-Hydroxymethyl-	3% (7%)	11% (8%)	0.16 (0.41)	0.32 (0.24)
12-crown-4)				
E2 (dibenzo-14-crown-4	5% (6%)	8% (9%)	0.20 (0.24)	0.40 (0.42)
ether)				
GO-Epi2-E1	68% (63%)	16% (18%)	1.11 (1.02)	0.22 (0.25)
GO-Epi2-E2	78% (76%)	17% (21%)	2.64 (2.62)	0.23 (0.32)
Chit-PVA	4% (4%)	6% (6%)	0.13 (0.16)	0.25 (0.23)
GO-Epi2-E1/Chit-PVA	22% (23%)	16% (16%)	0.40 (0.44)	0.35 (0.37)
GO-Epi1-E2/Chit-PVA	35% (37%)	16% (16%)	0.95 (0.98)	0.43 (0.45)

Effects of various parameters on Li⁺ extraction process

Certain amount of the synthesized DB14C4–C16 was dissolved in CH_2Cl_2 to serve as the organic phase in the solvent extraction experiments. The solution contains pure Li⁺ (200 mg/L).



Comparative Study on Lithium Recovery with Ion-Selective Adsorbents and Extractants: Results of Multi-Stage Screening Test with the Use of Brine Simulated Solutions with Increasing Complexity

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Stage Number	Li ⁺ [mg/kg]	Na ⁺ [wt%]	Ca ²⁺ [wt%]	Mg ²⁺ [mg/k	g]			
1	300	0	0	0				
2	300	0.10	0	0				
3	297	1.00	0	0				
4	240	7.86	0	0				
5	240	7.86	0.1	0				
6	220	7.21	3.0	0				
7	220	7.21	3.0	300				
8	220	7.21	3.0	1000				
Sample Name	R _{Li} 1 (R _{Li} 2 pH 9)	R _{Li} 2 (R _{Li} 2 pH 9)	R _{Li} 3 (R _{Li} 3 pH 9)	R _{Li} 4 (R _{Li} 4 pH 9)	R _{Li} 5 (R _{Li} 5 pH 9)	R _{Li} 6 (R _{Li} 6 pH 9)	R _{Li} 7 (R _{Li} 7 pH 9)	R _{Li} 8 (R _{Li} 8 pH 9)
		Oth	er commerciall	y available adso	orbents			
CellPhos	47.4%	33.3%	16.7% (16.7%)	x	x	x	х	х
SiO ₂ -Et/Bu- PO(OH) ₂	52.4%	60.0%	23.1% (33.3%)	9.1% (16.7%)	x	х	x	х
		Manga	nese oxide-bas	ed adsorbents (prepared)			
LIS10	37.5%	16.7% (>99.7%)	9.1% (>99.7%)	16.7% (>99.7%)	16.7% (>99.7%)	16.7% (>99.7%)	16.7% (>99.7%)	16.7% (>99.7%)
LIS11	33.3%	16.7% (>99.7%)	9.1% (>99.7%)	16.7% (>99.7%)	16.7% (>99.7%)	16.7% (>99.7%)	16.7% (>99.7%)	16.7% (93.2%)
LIS12	33.3%	16.7% (>99.7%)	33.3%	16.7% (>99.7%)	16.7% (>99.7%)	16.7% (>99.7%)	16.7% (>99.7%)	16.7% (96.8%)



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Thank you for attention

