

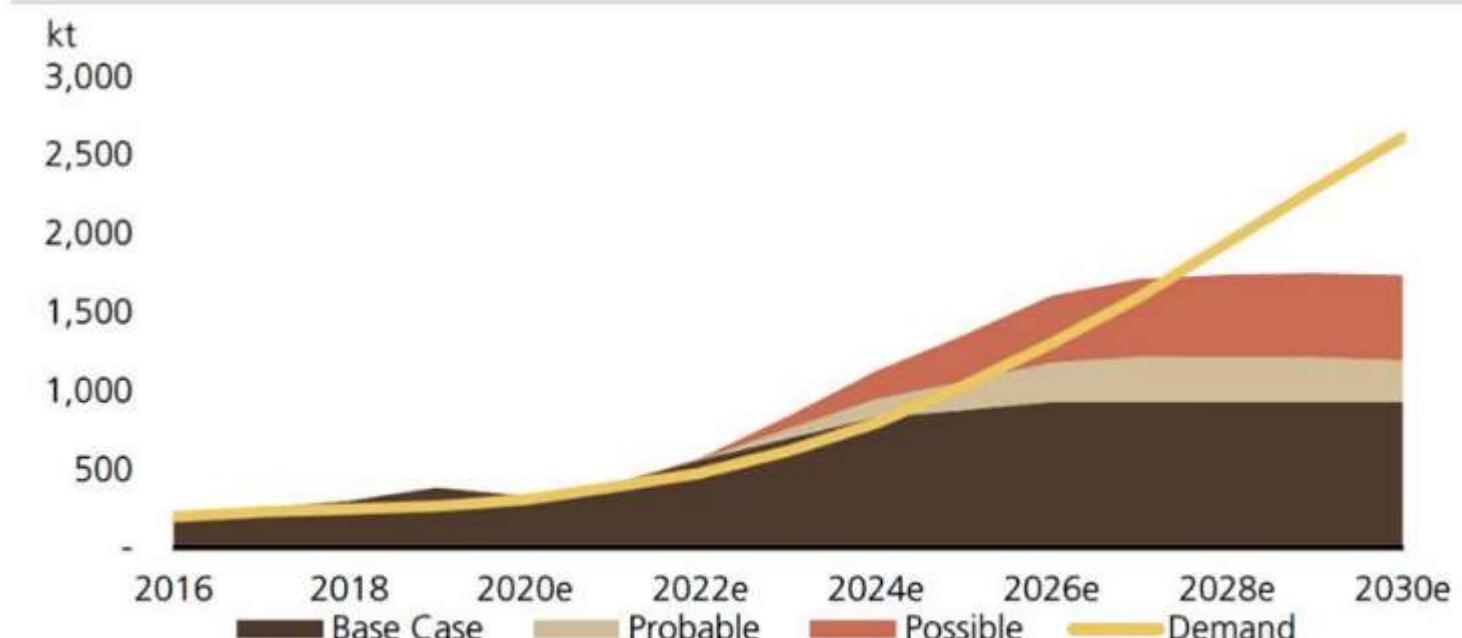
# Lithium extraction from natural brines through membrane electrolysis with limited waste generation.

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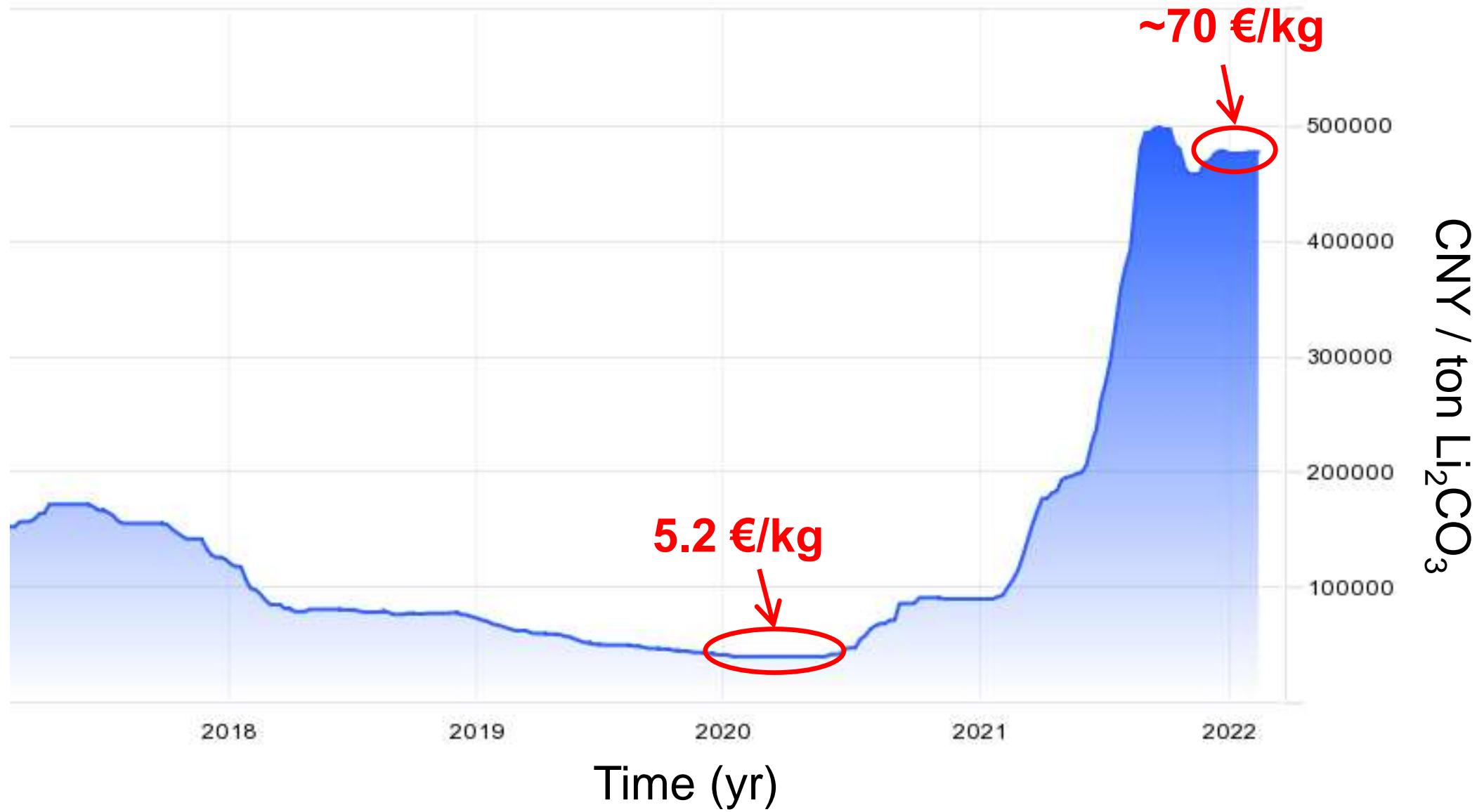
## Lithium supply – Demand balance



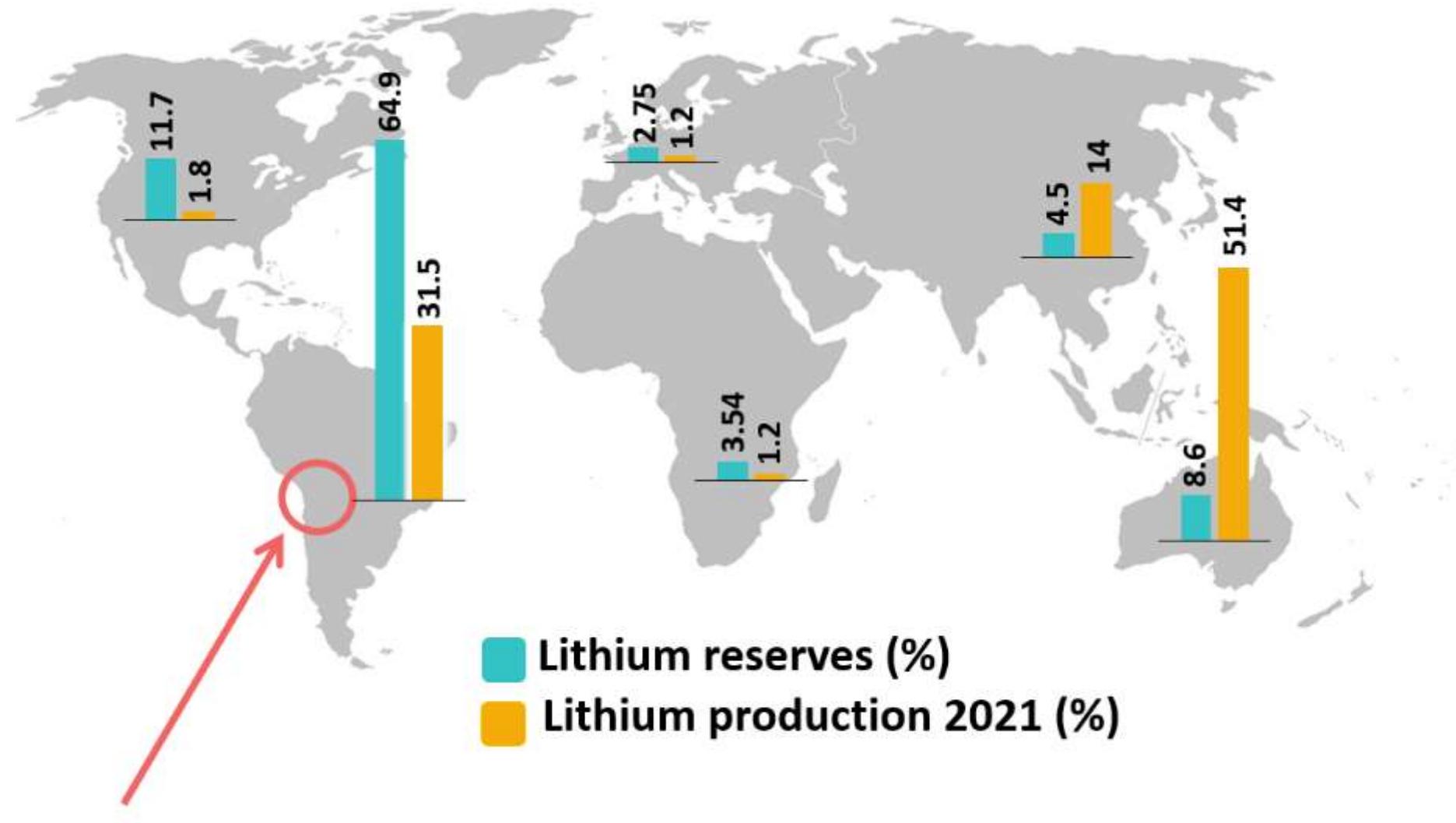
Source: WoodMac, Company Filings, UBSe.

Supply risk comes from **production capacity**

# Price $\text{Li}_2\text{CO}_3$



# Lithium distribution



Lithium triangle

# Lithium from brines

55-65% of the world's lithium resources.

Li brines = Na, K, Mg, Ca, B, SO<sub>4</sub>, Cl ...

~1-2 g/L Li



# HOW IS LITHIUM EXTRACTED FROM BRINES?

An aerial photograph of the Salar de Olaroz salt flat in Argentina. The vast, light-colored salt flats are visible in the foreground and middle ground, with a network of roads and industrial structures. In the background, there are green hills and mountains under a blue sky with scattered clouds.

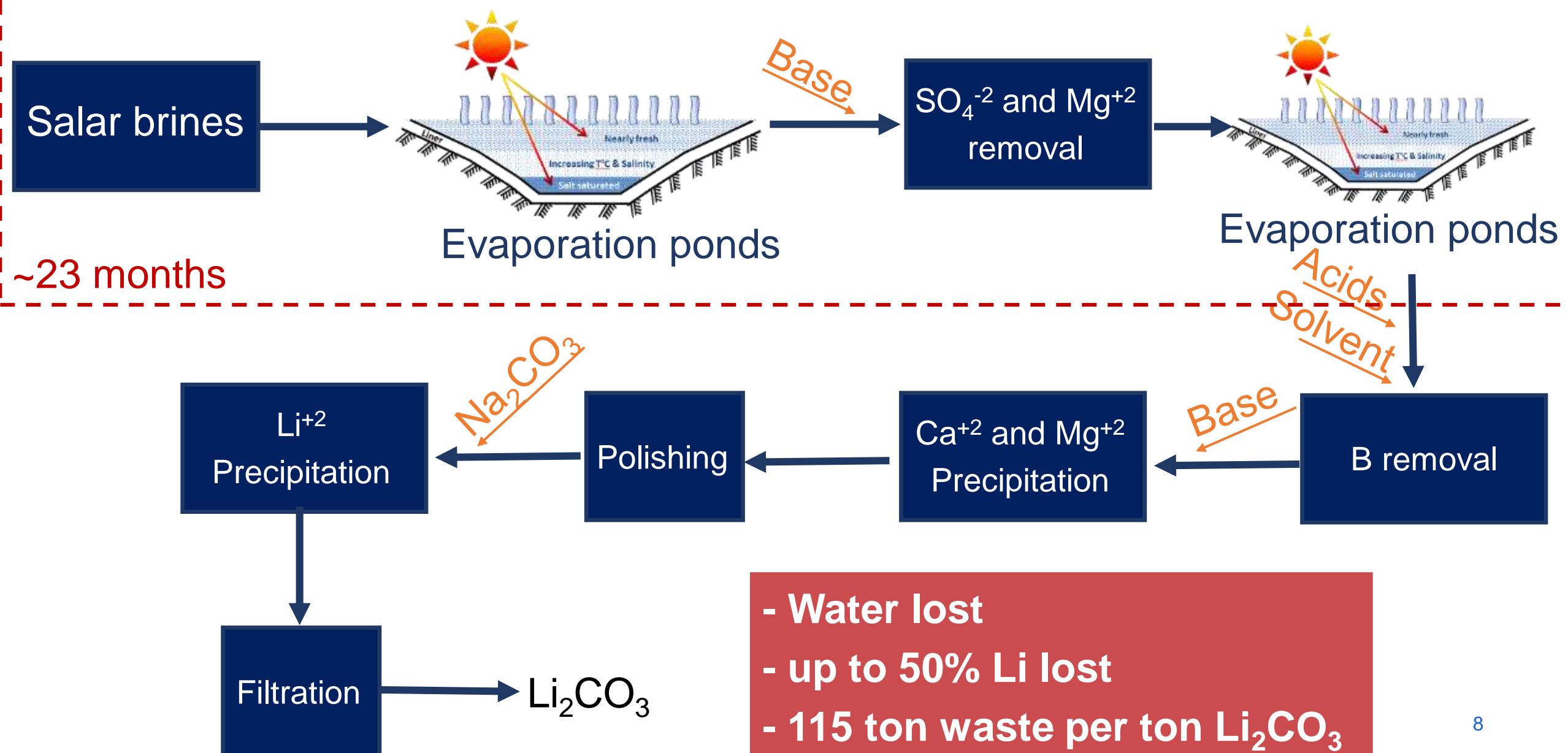
*Salar de Olaroz*

Current process:  
evaporation/precipitation in open-air ponds

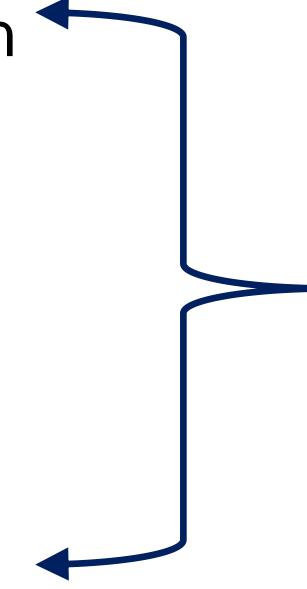
Solar evaporation



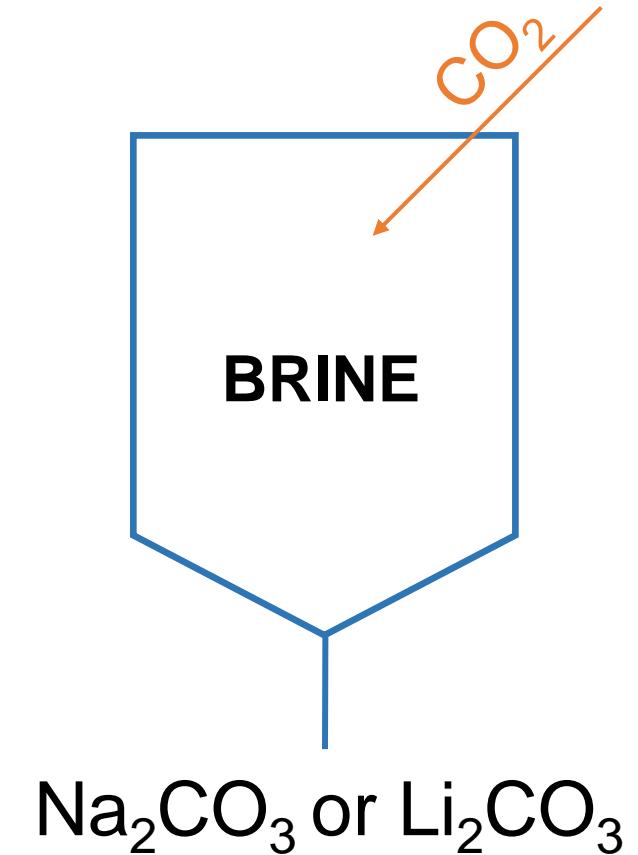
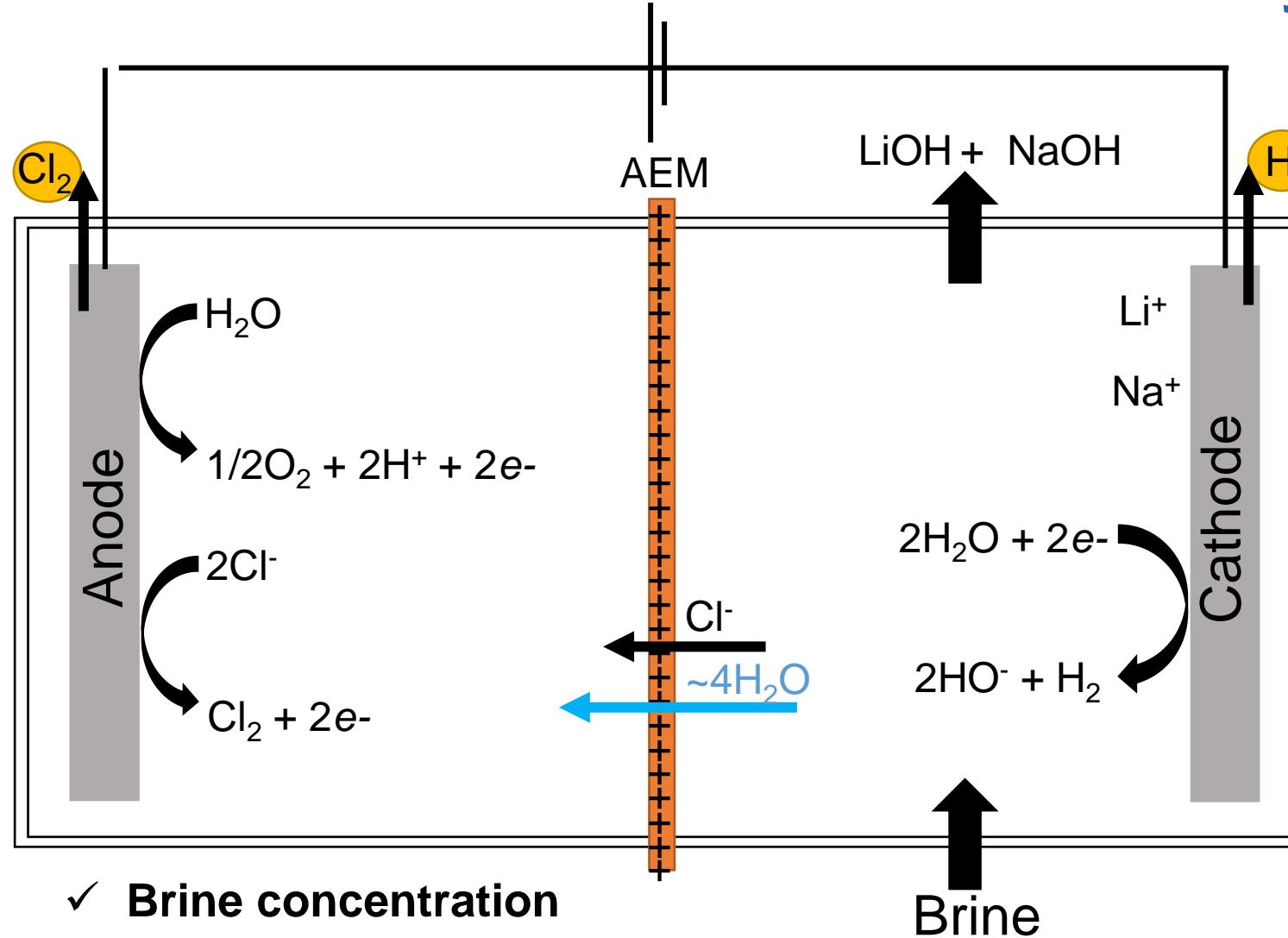
# Conventional brine processing based on natural evaporation



# Conventional brine processing based on natural evaporation

- Brine concentration - water evaporation
  - NaCl removal – water evaporation
  - Mg and Ca removal – base addition
  - B removal – acids + solvents addition
  - $\text{Li}_2\text{CO}_3$  precipitation -  $\text{Na}_2\text{CO}_3$  addition
- 
- ✓ **Brine concentration**
  - ✓ **Changes in pH**
  - ✓  **$\text{CO}_3^{2-}$  addition**

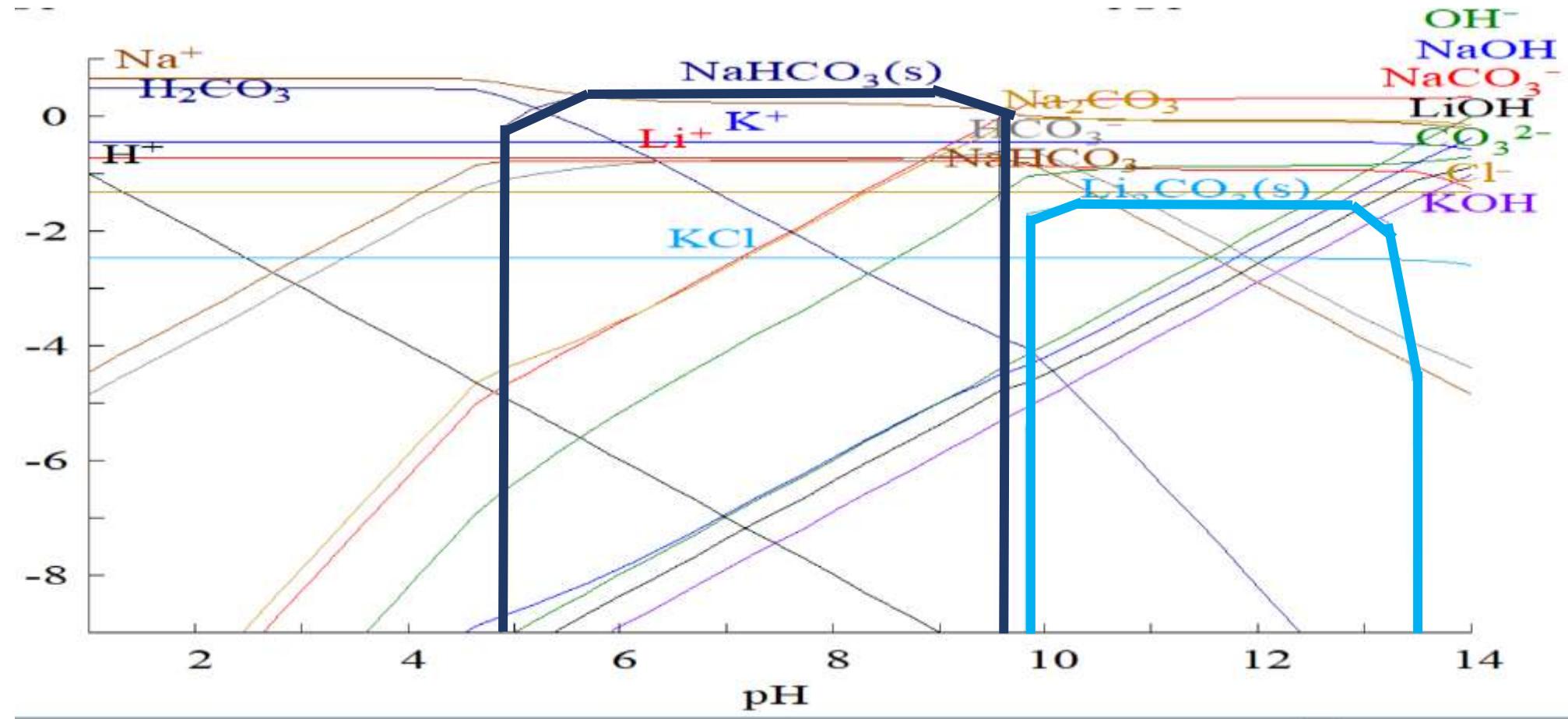
# Li+WATER - Membrane electrolysis



- ✓ Brine concentration
- ✓ Changes in pH
- ✓  $\text{CO}_3^{2-}$  addition

# Experimental design

$\text{Na}^+$ (M)	$\text{Li}^+$ (M)	$\text{K}^+$ (M)	$\text{Cl}^-$ (M)	$\text{SO}_4^{2-}$ (M)
4.86	0.19	0.36	5.15	0.11



# Li+WATER process - Experimental design

Brine composition (M)

$\text{Li}^+$  0.18

$\text{Ca}^{2+}$  0.02

$\text{Mg}^{2+}$  0.12

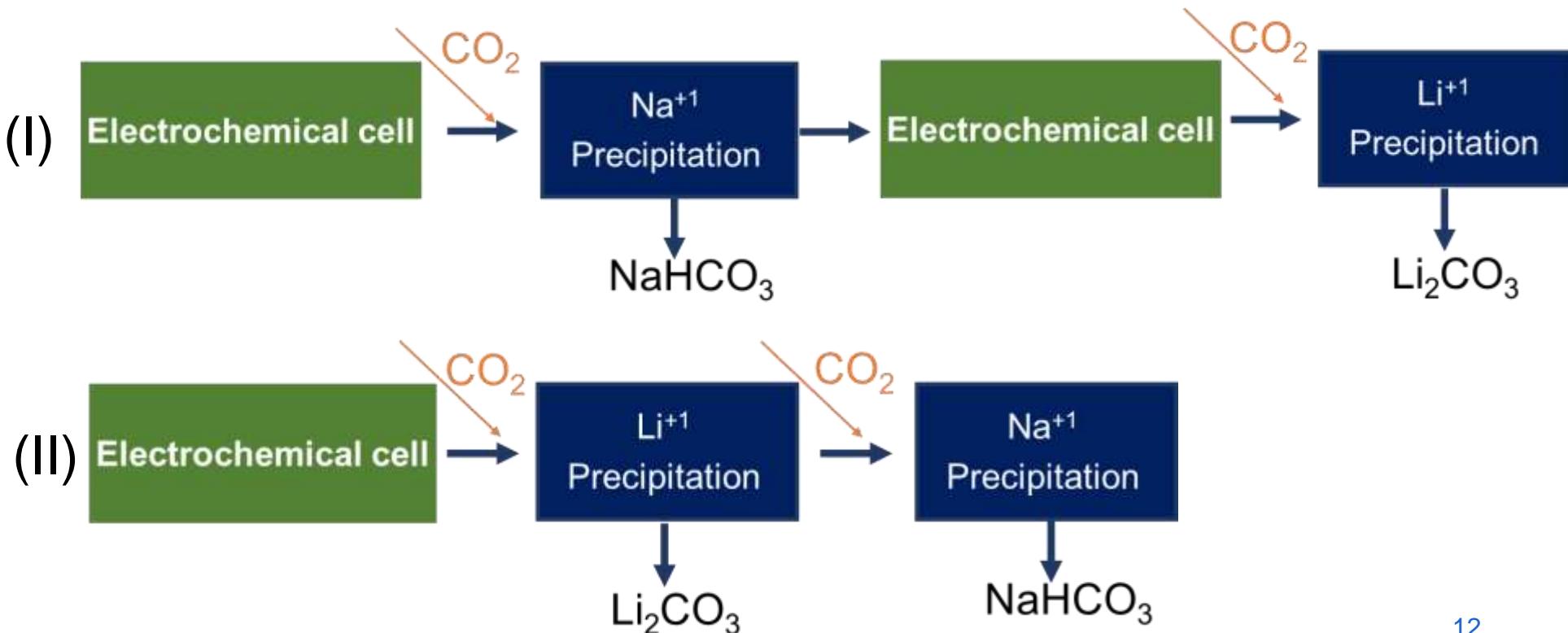
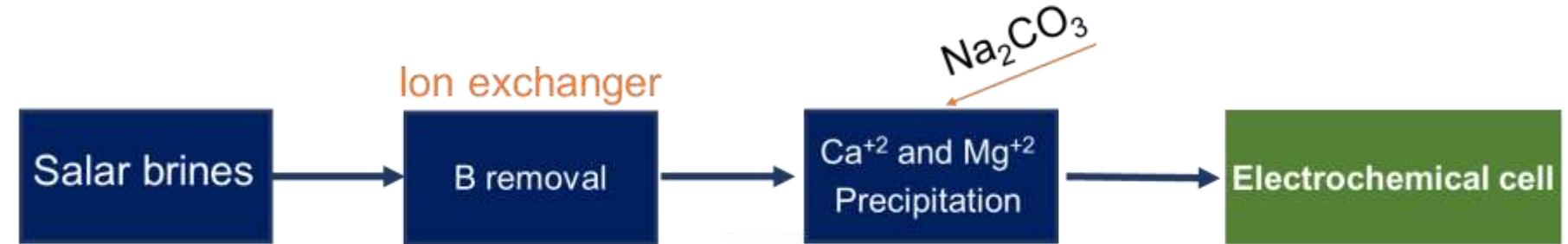
B 0.14

$\text{Na}^+$  4.49

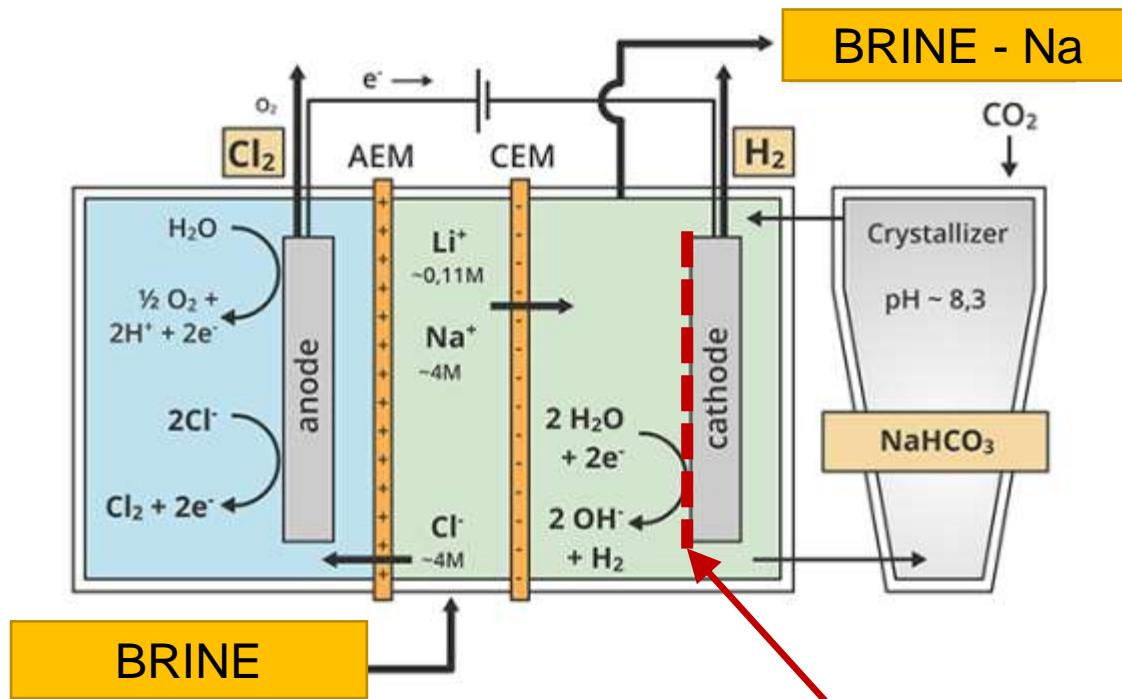
$\text{K}^+$  0.36

$\text{Cl}^-$  5.15

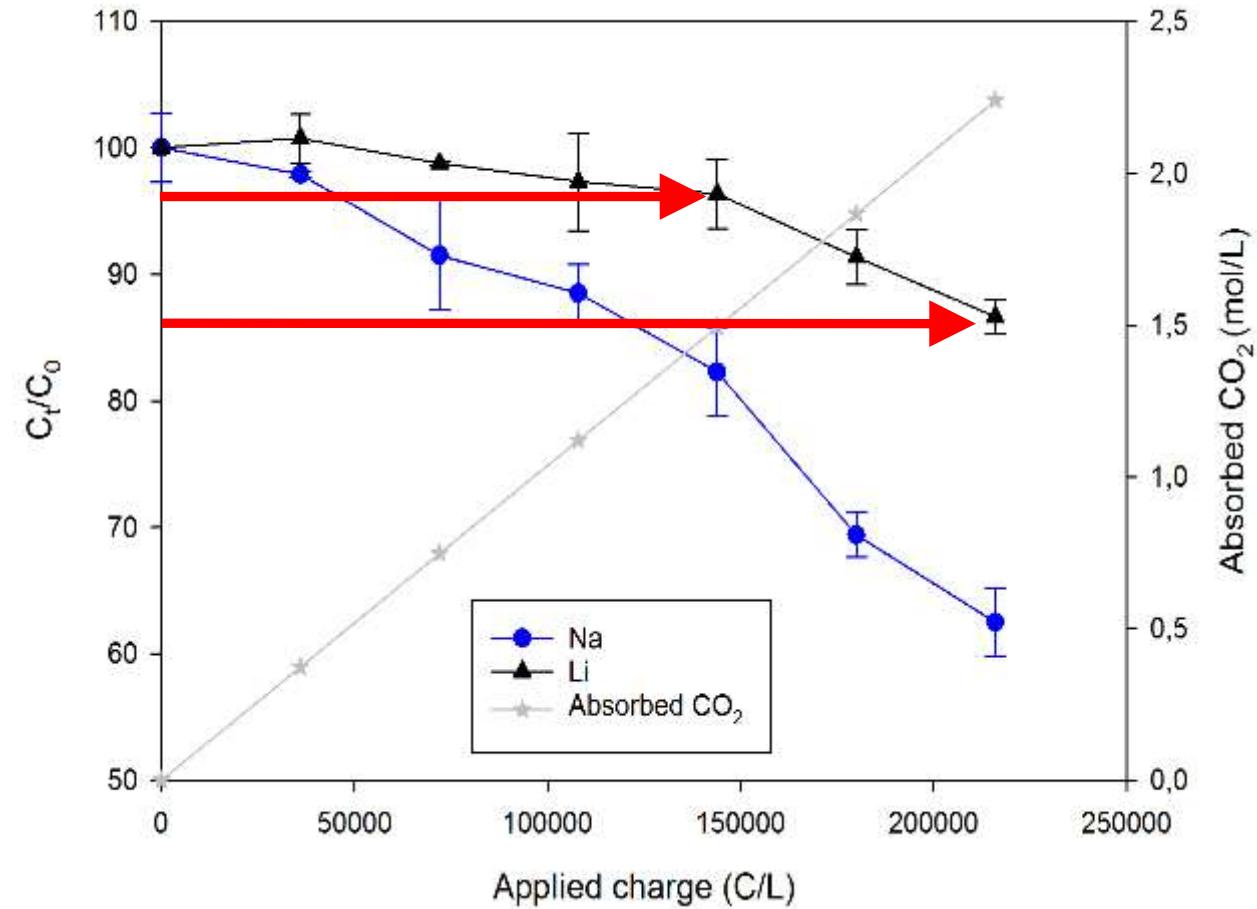
$\text{SO}_4^{2-}$  0.11



# (I) - Sodium bicarbonate precipitation



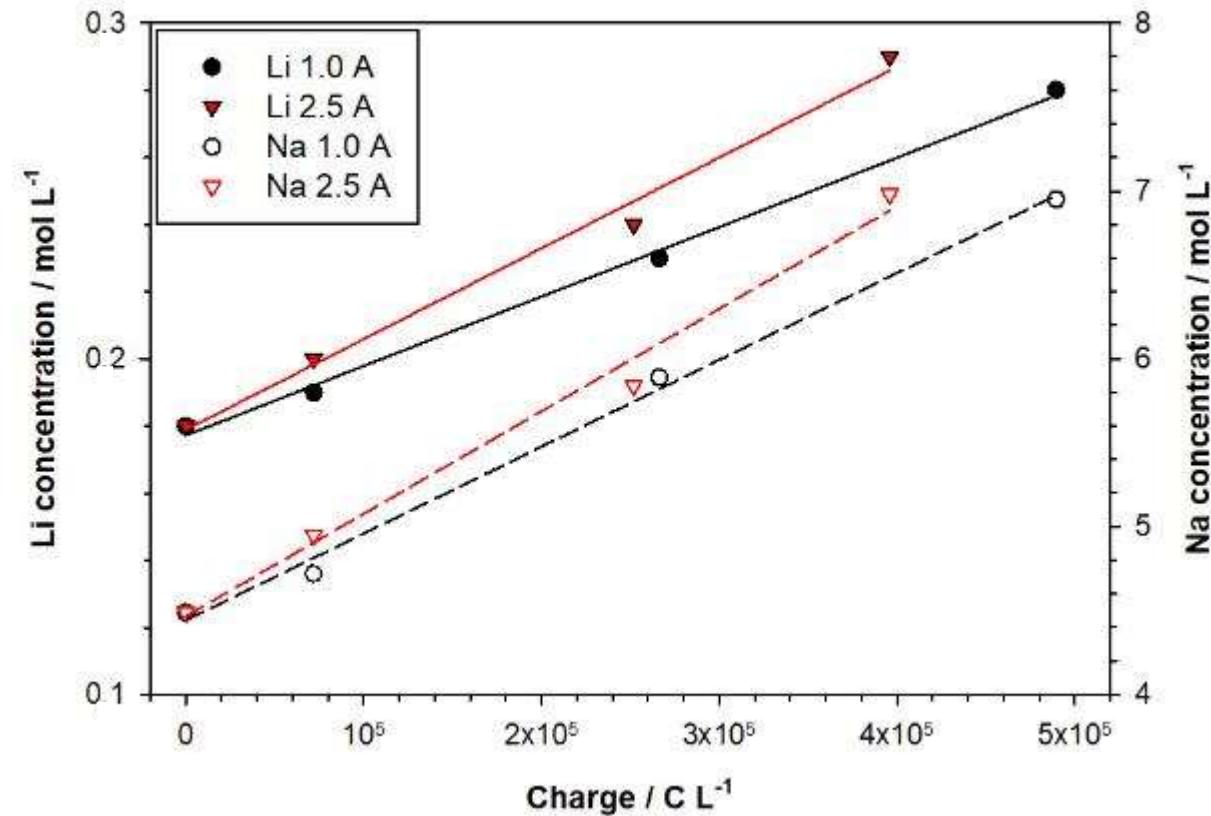
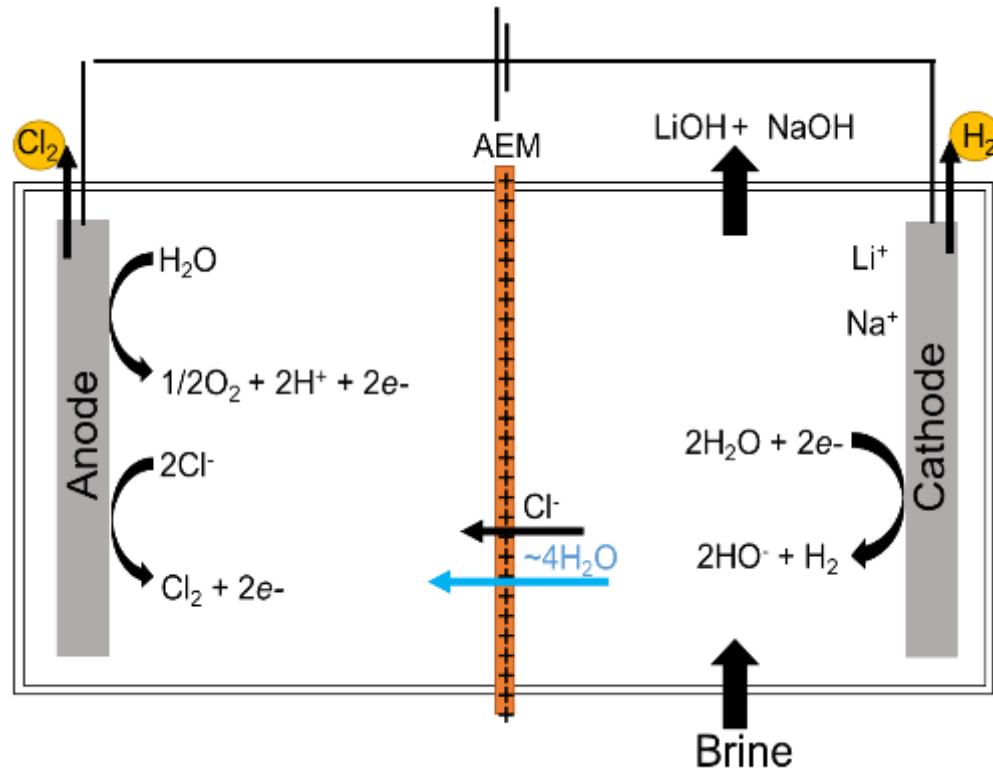
Higher pH in the  
cathode interface



- Lithium lost during Na extraction
- It is possible to extract Li first?

## (II) – Lithium carbonate precipitation

### $\text{OH}^-$ Generation



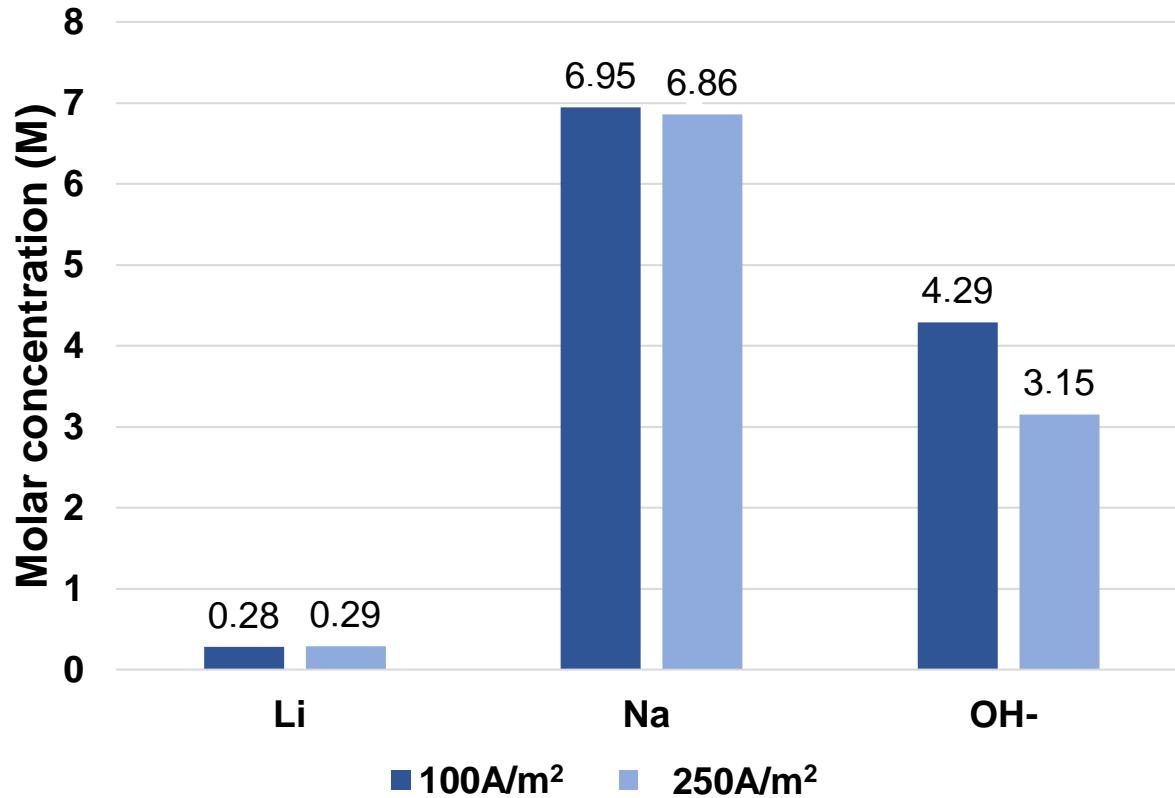
Li and Na concentration increase in the cathode

## (III) – Lithium carbonate precipitation

- Catholyte volume 650 mL
- Charge applied

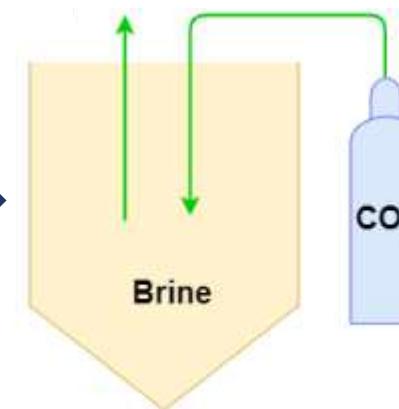
$$100\text{A/m}^2 = 489 \text{ kC}$$

$$250\text{A/m}^2 = 396 \text{ kC}$$



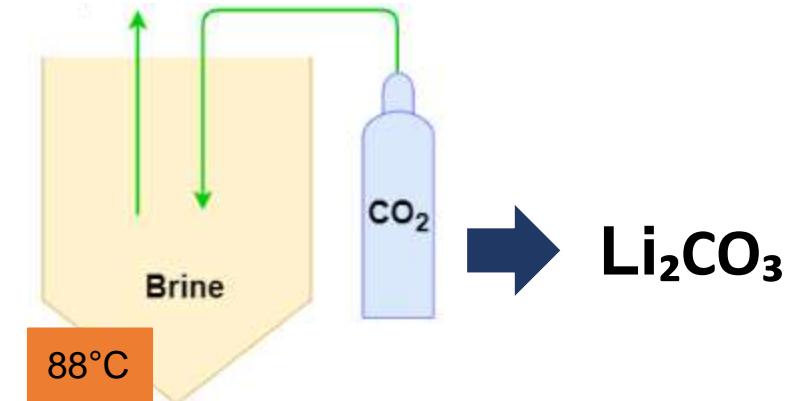
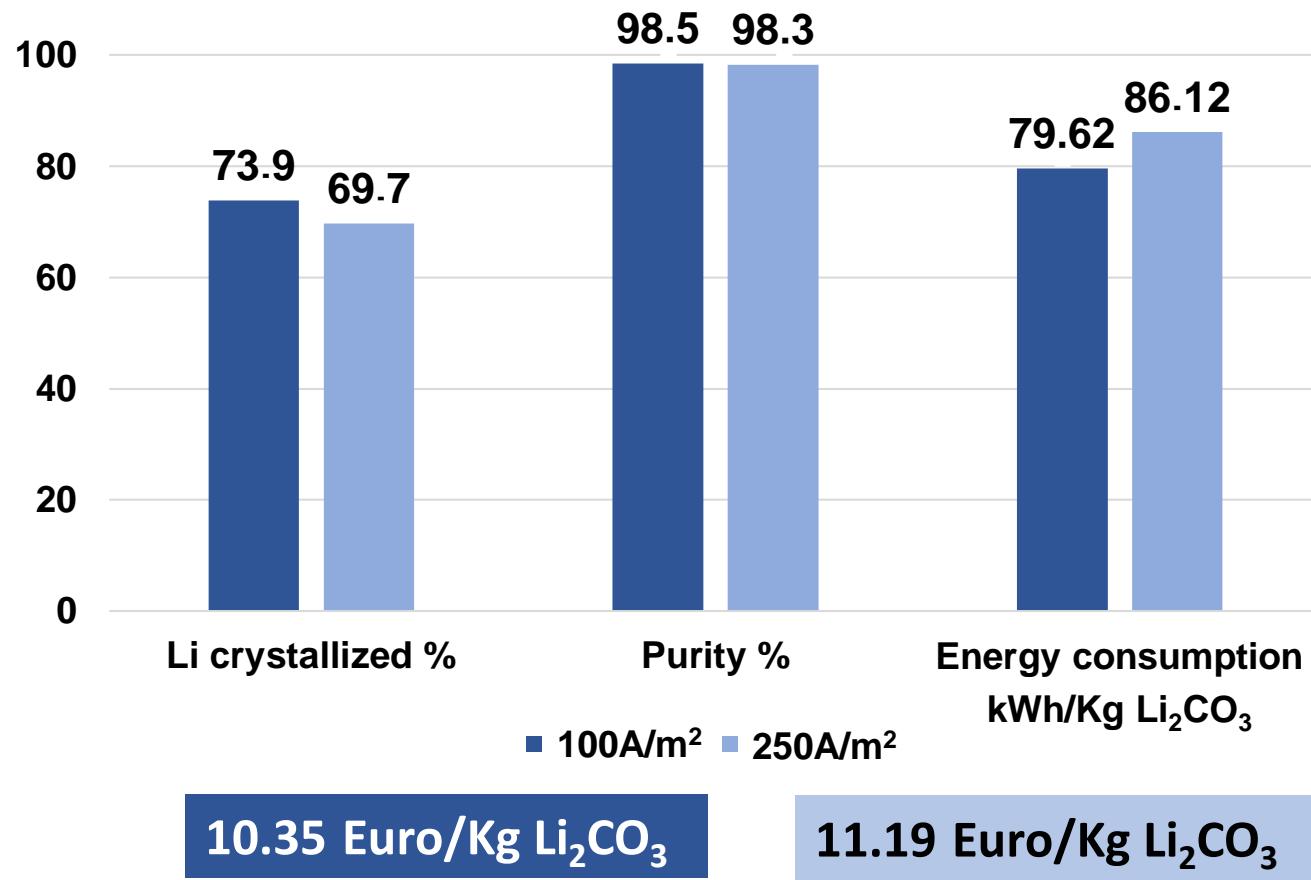
$\text{Li}_2\text{CO}_3$  crystallization

➤  $\text{CO}_2$  fluxing until pH 11- 88°C



$\text{Li}_2\text{CO}_3$

## (II) – Lithium carbonate precipitation



**100A/m<sup>2</sup>**

mol/L

Li<sup>+</sup> 0.07

Na<sup>+</sup> 7.02

**250A/m<sup>2</sup>**

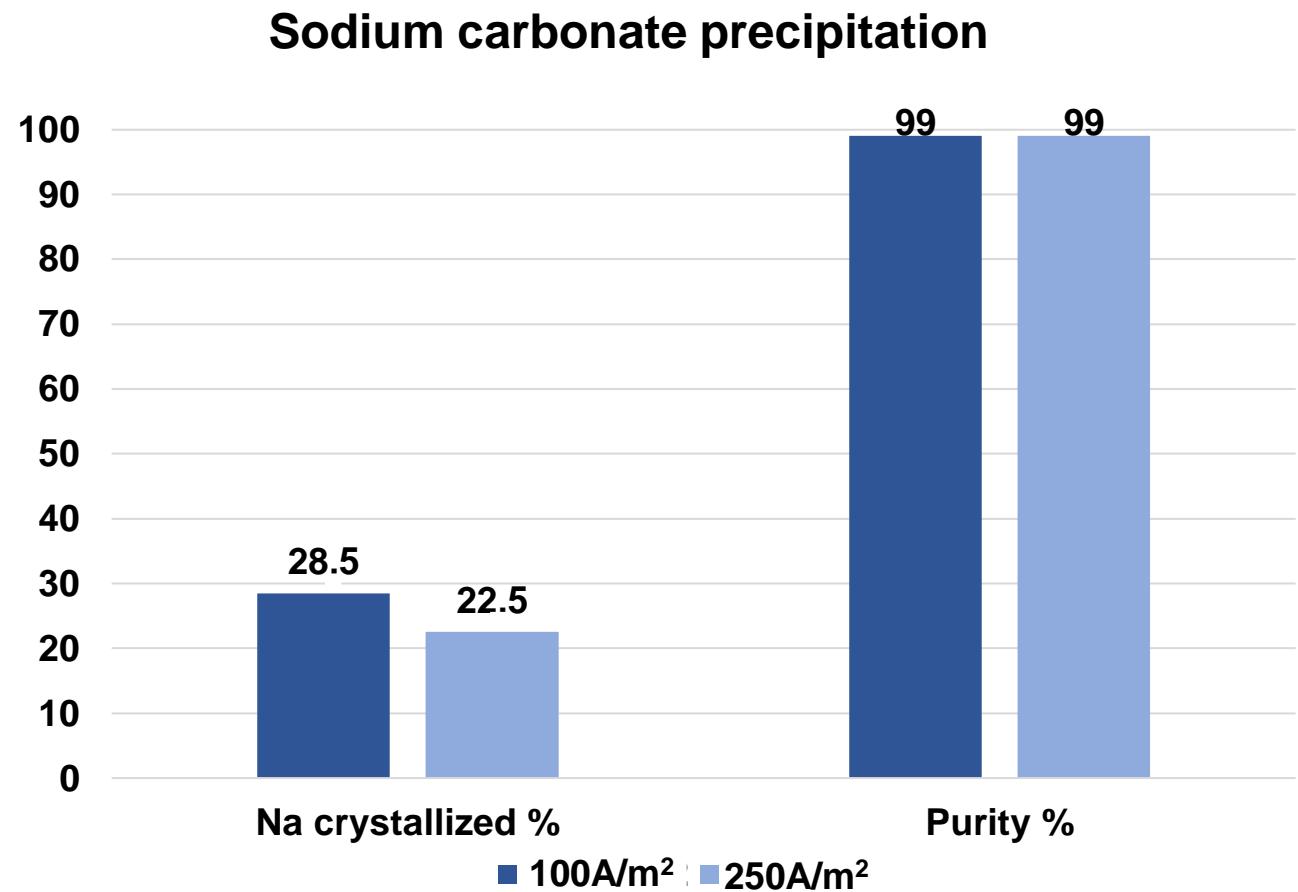
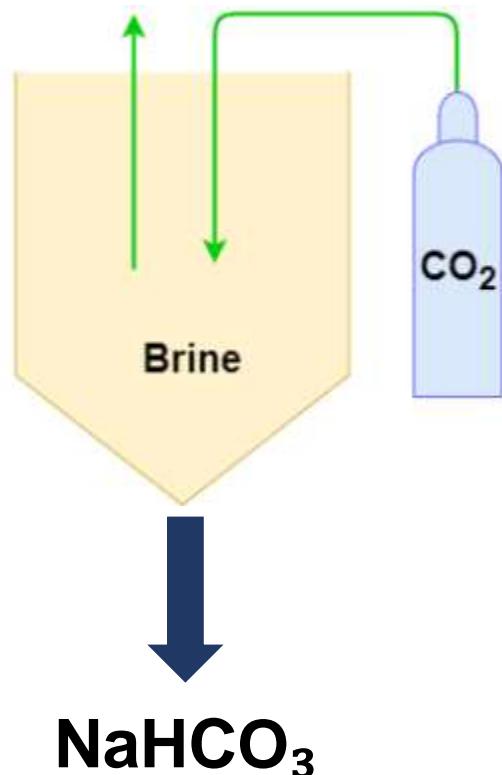
mol/L

Li<sup>+</sup> 0.08

Na<sup>+</sup> 7.02

## (II) – Sodium bicarbonate precipitation

- 20°C
- CO<sub>2</sub> fluxing until pH 8.5



1.9 kg Na<sub>2</sub>CO<sub>3</sub> / kg Li<sub>2</sub>CO<sub>3</sub>

# CONCLUSIONS

- ✓ **Membrane electrolysis based process**
- ✓ **Controllable and weather independant**
- ✓ **No water lost**
- ✓ **No chemicals except CO<sub>2</sub>**
- ✓ **Extraction of by-products / limited waste generation**
- ✓ **Energy cost still high**

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